# SOYBEAN BIOESTER OBTAINED IN A BUBBLE COLUMN ESTERIFICATION REACTOR – A RHEOLOGICAL STUDY

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**ABSTRACT.** The paper presents the rheological characterization of a bio-ester with possible lubricant properties, obtained from soybean oil fatty acids. The rheological characterization was carried out under thermostatic conditions, using a Brookfield CAP2000+L viscometer in the characteristic domain of these fluids. The variation of the apparent viscosity  $\eta_a$  as a function of shear rate  $\dot{\gamma}$  and the variation of the two indices (K and n) as a function of temperature were determined, as well as the flow activation energy,  $E_a$  from Arrhenius type equations. A rheological model was proposed.

Keywords: apparent viscosity, fatty acids, non-Newtonian behavior

### INTRODUCTION

At present time, environmental protection as well as concerns regarding future energetic security have become of prime importance. That is why the use of bio-based lubricants is important in the transport and industrial sectors, to the detriment of classic synthetic lubricants.

With proper formulation of the base oil and with proper use of additive packages, bio-based lubricants can work better than conventional lubricants [1].

It is important to study the rheological properties of lubricating products, with or without additions of various additives, in order to know their tribological behavior [2-8].

Environmental protection is at present a very important issue [9]. That is why eco-friendly technologies are to be used for protecting the environment. Esterification processes can be performed in bubble column reactors, which were also used in different technologies, such as polymerization processes, when the residual monomer did not appear in the final product [10-14] and the heat transfer may be monitored by the boiling heat transfer coefficients [15-18].

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As a continuation of research undertaken in previous years [19-24], at present we aim to obtain lubricating products that do not affect the environment, but which have superior lubricating properties, using bubble column reactors technologies.

For this purpose, it was obtaining a bio-ester with possible lubricating properties using as acid component the soybean oil fatty acids, *n*-propanol and *p*-toluene-sulphonic acid as catalyst, in a bubble column reactor. The rheological behavior of the bio-ester was studied.

## **RESULTS AND DISCUSSION**

Some physico-chemical properties of the bio-ester are presented in Table 1.

Property	Value
Appearance	viscous, opalescent
Color	orange
Acidity index, mg KOH g <sup>-1</sup>	< 1
Refractive index, (20°C)	1.4562
Density (25°C), g cm <sup>-3</sup>	0.9981

Table 1. Some physico-chemical properties of the bio-ester

The variation of the apparent viscosity  $\eta_a$  as a function of shear rate  $\dot{\gamma}$ , at different temperature values, is shown in Figure 1.



Shear rate, 1/s

Figure 1. Apparent viscosity vs. shear rate for bio-ester at different temperature values

It is noticed that the values of the apparent viscosity decrease with the shear rate increasing, behavior that is characteristic of non-Newtonian fluids (shear-thinning behavior). The dependence  $\eta_a = f(\dot{\gamma})$  can be described by the equation Ostwald de Waele, equation (1):

$$\eta_a = K \cdot \dot{\gamma}^{n-1} \tag{1}$$

where: K – the flow consistency index,  $Pa \cdot s^n$ ; n – the flow behavior index [25,26].

The particular forms of equation (1), corresponding to the five temperature values, are shown in Table 2.

Temperature, °C	$\eta_a = f(\dot{\gamma})$	R <sup>2</sup>
25	$\eta_a = 0.19 \cdot \dot{\gamma}^{-0.234}$	0.9191
35	$\eta_a = 0.15 \cdot \dot{\gamma}^{-0.219}$	0.9343
50	$\eta_a = 0.164 \cdot \dot{\gamma}^{-0.24}$	0.9836
60	$\eta_a = 0.103 \cdot \dot{\gamma}^{-0.198}$	0.9740
70	$\eta_a = 0.058 \cdot \dot{\gamma}^{-0.147}$	0.9658

**Table 2.** Particular forms of equation (1)

The pseudoplastic behavior is also demonstrated by the sub-unit values of the flow behavior index.

The variation of the two indices (K, n) as a function of temperature is shown in Figure 2, and in Figure 3 is presented the variation of the apparent viscosity with temperature, for three values of the shear rate.



Figure 2. The material consistency and flow behavior index vs. temperature



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Figure 3. Apparent viscosity vs. temperature at different shear rate values

The temperature increase leads to microdrops mobility intensification which influences the activation energy of the system. The phenomenon can be explained by an Arrhenius type equation (equation (2)):

$$\eta_a = A' \cdot e^{\frac{E_a}{R \cdot T}} \tag{2}$$

where  $E_a$  is the activation energy of viscous flow, J mol<sup>-1</sup>; *R* is the gas general constant, J mol<sup>-1</sup> K<sup>-1</sup>; *T* is absolute temperature and *A*' represents the material constant, Pa s. The dependence  $\ln\eta_a = f(1/T)$  was graphically represented, as obtained from the logarithmic form of equation (2), for apparent viscosity values corresponding to the three chosen values of the shear rate. Particular expressions of equation (2) as well as the values of the activation energy are presented in Table 3.

<sup>γ</sup> , s <sup>-1</sup>	$\eta_a = A' \times 10^4 \cdot \exp(\frac{E_a}{R \cdot T})$	$E_a, kJ \cdot mol^{-1}$
4000	$\eta_a = 6.6 \cdot exp(\frac{1130.7}{T})$	9.4
9333	$\eta_a = 11.9 \cdot exp(\frac{886.2}{T})$	7.4
13333	$\eta_a = 18.4 \cdot exp(696.6/T)$	5.8

 Table 3. Particular forms of equation (2)

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### CONCLUSIONS

It was studied the rheological behavior of a bio-ester obtained from soybean oil fatty acids in the bubble column reactor at reflux.

The synthesized ester exhibits pseudoplastic behavior characterized by the decrease in apparent viscosity with the shear rate increasing and subunit values of the flow behavior index. These values increase with increasing temperature, without exceeding the value 1.

It is also observed that the activation energy of viscous flow decreases with the shear rate increasing.

### **EXPERIMENTAL SECTION**

#### General procedure for ester preparation

Synthesis of the bio-ester was performed in the bubble column reactor at reflux. The ratio fatty acids from soybean oil: n-propanol was 1:2, using 0.4% catalyst [17-22].

The physico-chemical properties were determined by using standardized techniques: the pycnometer method for density determination and the Abbe refractometer for refractive indices.

The rheological characterization of the samples was carried out under thermostatic conditions (temperature range 25÷70°C), using a Brookfield CAP2000+L viscometer in the characteristic domain of these fluids.

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